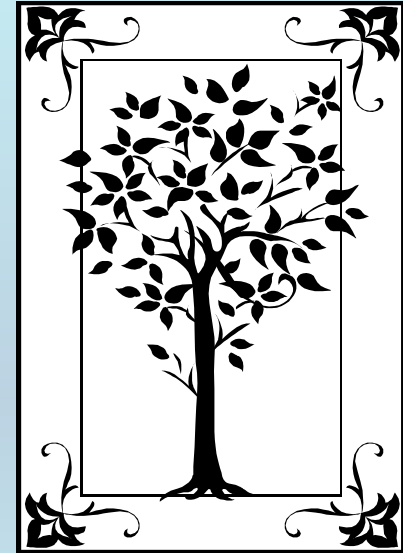


# METADATA AND NUMERICAL DATA CAPTURE:

$$\text{DENSITY} = f(T, p, x)$$

**2 – Components and 1 Phase**

## *Guided Data* **Capture (GDC)**



This tutorial describes  
METADATA AND NUMERICAL DATA CAPTURE:  
for **2-components and 1 phase**  
**DENSITY (kg/m<sup>3</sup>)**  
with the Guided Data Capture (GDC) software.

## **NOTE:**

The tutorials proceed sequentially to ease the descriptions. **It is not necessary to enter *all* compounds before entering *all* samples, etc.**

Compounds, samples, properties, etc., can be added or modified at any time.

**However, the hierarchy must be maintained** (i.e., a property cannot be entered, if there is no associated sample or compound.)

The experimental data used in this example is from:

*J. Chem. Eng. Data* 2002, 47, 233–238

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## High-Pressure Volumetric Behavior of $x$ 1,1,1,2-Tetrafluoroethane + $(1 - x)$ 2,5,8,11,14-Pentaoxapentadecane (TEGDME) Mixtures

María J. P. Comuñas,<sup>†‡</sup> Antoine Baylaucq,<sup>‡</sup> Christian Boned,<sup>‡</sup> Xavier Canet,<sup>‡</sup> and Josefa Fernández<sup>\*†</sup>

Laboratorio de Propiedades Termofísicas, Departamento de Física Aplicada, Facultad de Física, Universidad de Santiago de Compostela, E-15782 Santiago de Compostela, Spain, and Laboratoire des Fluides Complexes, Faculté des Sciences, BP 1155, F-64013 Pau Cedex, France

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This paper reports 1017 new  $pVT$  measurements of the  $x$  1,1,1,2-tetrafluoroethane (HFC-134a) +  $(1 - x)$  2,5,8,11,14-pentaoxapentadecane (TEGDME) system for  $x = 0.0, 0.1114, 0.2896, 0.3648, 0.5702, 0.6931, 0.7288, 0.8727, 0.9290,$  and 1 between 10 and 60 MPa in the temperature range 293.15 K to 373.15 K at 5 MPa and 10 K intervals, respectively. In almost all the measurement range, the density of the pure compressed refrigerant is greater than that of the pure polyether. For temperatures higher than 343.15 K, the isocomposition curves for the mixtures show an intersection point. Similar behavior has been previously found for HFC-134a + triethylene glycol dimethyl ether, carbon dioxide + alkane or toluene systems, and mixtures of R-410A with polyolester lubricants. The excess molar volume is negative over the whole composition range at all temperatures and pressures.

---

# DENSITY = $f(T, p, x)$

(2 ñ Components)

1,1,1,2-Tetrafluoroethane (HFC 134a) + 2,5,8,11,14-Pentaoxapentadecane (TEGDME)

Table 1. Experimental Values of Densities,  $\rho$ , for  $x$  HFC-134a + (1 -  $x$ ) TEGDME at Different Temperatures,  $T$ , and Pressures,  $p$

$x$	$p/\text{MPa}$	$\rho/(\text{g}\cdot\text{cm}^{-3})$ at the following values of $TK$									
		293.15	303.15	313.15	323.15	333.15	343.15	353.15	363.15	373.15	
0	0.1	1.0112	1.0018	0.9925	0.9833	0.9740	0.9648	0.9556	0.9469	0.9375	
	5	1.0142	1.0050	0.9959	0.9868	0.9778	0.9687	0.9598	0.9513	0.9423	
	10	1.0172	1.0082	0.9992	0.9903	0.9814	0.9726	0.9639	0.9557	0.9468	
	15	1.0201	1.0113	1.0025	0.9937	0.9850	0.9764	0.9679	0.9598	0.9511	
	20	1.0229	1.0143	1.0055	0.9970	0.9883	0.9800	0.9716	0.9639	0.9552	
	25	1.0257	1.0172	1.0086	1.0001	0.9917	0.9835	0.9752	0.9675	0.9593	
	30	1.0284	1.0200	1.0116	1.0032	0.9950	0.9869	0.9788	0.9712	0.9631	
	35	1.0310	1.0227	1.0144	1.0063	0.9982	0.9901	0.9821	0.9748	0.9669	
	40	1.0336	1.0254	1.0172	1.0091	1.0012	0.9932	0.9855	0.9783	0.9704	
	45	1.0361	1.0281	1.0201	1.0121	1.0042	0.9963	0.9886	0.9815	0.9739	
	50	1.0385	1.0306	1.0226	1.0147	1.0070	0.9993	0.9917	0.9846	0.9771	
	55	1.0410	1.0332	1.0252	1.0175	1.0098	1.0023	0.9947	0.9880	0.9805	
	60	1.0434	1.0355	1.0278	1.0202	1.0126	1.0050	0.9976	0.9910	0.9838	
	0.1114	10	1.0315	1.0220	1.0124	1.0031	0.9936	0.9844	0.9752	0.9659	0.9564
15		1.0345	1.0254	1.0159	1.0067	0.9975	0.9887	0.9794	0.9704	0.9611	
20		1.0375	1.0285	1.0192	1.0103	1.0011	0.9925	0.9834	0.9746	0.9657	
25		1.0405	1.0316	1.0223	1.0136	1.0047	0.9962	0.9872	0.9787	0.9699	
30		1.0433	1.0346	1.0255	1.0169	1.0081	0.9998	0.9911	0.9828	0.9742	
35		1.0461	1.0374	1.0286	1.0201	1.0116	1.0032	0.9947	0.9866	0.9779	
40		1.0488	1.0403	1.0316	1.0232	1.0148	1.0065	0.9983	0.9903	0.9817	
45		1.0515	1.0431	1.0345	1.0263	1.0179	1.0099	1.0017	0.9937	0.9854	
50		1.0541	1.0457	1.0374	1.0291	1.0210	1.0129	1.0050	0.9972	0.9890	
55		1.0567	1.0485	1.0401	1.0321	1.0241	1.0162	1.0083	1.0006	0.9926	
60		1.0593	1.0510	1.0430	1.0349	1.0269	1.0189	1.0114	1.0038	0.9955	
0.2896		10	1.0563	1.0460	1.0357	1.0254	1.0151	1.0048	0.9945	0.9842	0.9739
		15	1.0598	1.0497	1.0396	1.0293	1.0190	1.0087	0.9984	0.9881	0.9778
		20	1.0632	1.0533	1.0434	1.0331	1.0228	1.0125	1.0022	0.9919	0.9816
	25	1.0665	1.0568	1.0470	1.0367	1.0264	1.0161	1.0058	0.9955	0.9852	
	30	1.0697	1.0601	1.0506	1.0403	1.0300	1.0197	1.0094	0.9991	0.9888	
	35	1.0728	1.0634	1.0540	1.0437	1.0334	1.0231	1.0128	1.0025	0.9922	
	40	1.0759	1.0666	1.0573	1.0470	1.0367	1.0264	1.0161	1.0058	0.9955	
	45	1.0788	1.0697	1.0606	1.0503	1.0400	1.0297	1.0194	1.0091	0.9988	
	50	1.0818	1.0727	1.0637	1.0534	1.0431	1.0328	1.0225	1.0122	1.0019	
	55	1.0846	1.0757	1.0668	1.0565	1.0462	1.0359	1.0256	1.0153	1.0050	
	60	1.0874	1.0785	1.0699	1.0613	1.0528	1.0443	1.0359	1.0277	1.0194	

These data are considered here. The complete data set is very extensive. Only this portion is used in the example, here.

## **Experimental Method Info:**

**Vibrating-tube densimeter**

**Uncertainty in density = 0.0002 g/cc**

**Uncertainty in temperature = 0.05 K**

**Uncertainty in pressure = 0.05 MPa**

## Guided Data Capture - Thermophysical and Thermochemical Data

File Edit Tools Help

Reference

Compound

Sample

Mixture

Reaction

Property

Data Tables

2002 com bay 0

1,1,1,2-tetrafluoroethane

Sample 1 (cm,99.94x%,nc;ns;)

^2: VDN (L), Set 1, B Method:VIBTLIB dVDN=0.0002 dP=50 dT=

2,5,8,11,14-pentaoxapentadecane

Sample 1 (cm,99x%,nc;ns;)

^2: VDN (L), Set 1, B Method:VIBTLIB dVDN=0.0002 dP=50 dT=

2,5,8,11,14-pentaoxapentadecane + 1,1,1,2-tetrafluoroethane

2. CLICK  
*Property*

1. SELECT the *mixture* for which the data are to be captured.

**NOTE:** The **bibliographic information**, **compound identities**, **sample descriptions**, and **mixture** were entered previously. (There are separate tutorials, which describe capture of this information, if needed.)

Property and experimental method for 2,5,8,11,14-pentaoxapentadecane + 1,1,1,2-tetrafluoroetha... Help

Property group: Volumetric properties

Property: Specific density

Units: g/cm3

Method of measurement:

Experimental purpose:

Comment (optional)

Property as function of state variable(s)

Invariant Property (No state variables)

Cancel

1. SELECT the **Property Group**: *Volumetric properties* from the menu.

2. SELECT the **Property**: *Specific density*, for the example.

3. SELECT the **Units**: g/cc

1. SELECT **Method of Measurement** from the list provided. **NOTE:** *Other* can be a valid selection and should include a brief description in the **Comment** field.

Method of measurement: Vibrating tube method

Experimental purpose: Principal objective of the work

2. SELECT the **Experimental Purpose** from the list provided.

Comment (optional)

Property as function of state variable(s)

Invariant Property (No state variables)

3. CLICK *Property as function of state variable(s)*

Cancel



**Experiment details**

Select the statements, which are true for the reported measurement

More than two calibration points used

Accept

**NOTE:** For some methods,  
additional information is  
requested.

# SELECTION of # of Phases in Equilibrium and # of Constraints

Specific density (g/cm<sup>3</sup>) as function of 3 variable(s)

Mixture: 2,5,8,11,14-pentaoxapentadecane + 1,1,1,2-tetrafluoroethane

Phases in equilibrium:

1

Constraints:

0

Independent variables:

3

Phase of the Property Value(s)

SELECT the # of **Phases in equilibrium**. There is **1** in the example; *liquid*.

SELECT the # of **Constraints** (such as *temperature, pressure, or composition*). There are none in the example.

Specific density (g/cm<sup>3</sup>) as function of 3 variable(s)

Mixture: 2,5,8,11,14-pentaoxapentadecane + 1,1,1,2-tetrafluoroethane

Phases in equilibrium: 1 Constraints: 0 Independent variables: 3 Property set #: 1

Sample #: 1 Sample #: 1

Phase of the Property Value(s):

Precision of the Property Value(s): g/cm<sup>3</sup> %

Definition of Measurement Results (Absolute vs Relative):

Data presentation: Experimental values

Comments (Optional):

Property and method Numerical Data Cancel

**Multiple *samples* for a given component can be accommodated, but this is rarely needed.**

Specific density (g/cm<sup>3</sup>) as function of 3 variable(s)

Mixture: 2,5,8,11,14-pentaoxapentadecane + 1,1,1,2-tetrafluoroethane

Phases in equilibrium: 1 Constraints: 0 Independent variables: 3 Property set #: 1 Sample #: 1 Sample #: 1

Phase of the Property Value(s) Liquid

Precision of the Property Value(s) g/cm<sup>3</sup>

Independent variable 1 Liquid

Independent variable 2 Liquid

Independent variable 3 Liquid

Definition of Measurement Results (Absolute / Relative)

**NOTE: Constraint and Independent Variable** field(s) appear automatically based on the entered information and the *Gibbs Phase Rule*.

1) SELECT *Liquid* from the list provided for the **Phase of the Property Value**

1. SELECT the **Independent Variable(s)** from the menus.

Specific density (g/cm<sup>3</sup>) as function of 3 variable(s)

Mixture: 2,5,8,11,14-pentaoxapentadecane + 1,1,1,2-tetrafluoroethane

Phases in equilibrium: 1 Constraints: 0 Independent variables: 3 Property set #: 1 Sample #: 1 Sample #: 1

Phase of the Property Value(s): Liquid Precision of the Property Value(s): 0.0002 g/cm<sup>3</sup>

Independent variable	Phase	Units	Uncertainty
Mole fraction of 1,1,1,2-tetrafluoroethane	Liquid	Dimensionless	
Pressure	Liquid	MegaPa	0.05
Temperature	Liquid	K	0.05

Definition of Measurement Results (Absolute/Relative):

Data presentation: Experimental values

Comments (Optional):

Property and method Numerical Data Cancel

2. SELECT **Units** for the Variable(s). Include approximate **Uncertainties**, if known.

Specific density (g/cm<sup>3</sup>) as function of 3 variable(s)

Mixture: 2,5,8,11,14-pentaoxapentadecane + 1,1,1,2-tetrafluoroethane

Phases in equilibrium: 1 Constraints: 0 Independent variable

Phase of the Property Value(s) Liquid

Independent variable 1  
Mole fraction of 1,1,1,2-tetrafluoroethane of Liquid

Independent variable 2  
Pressure of Liquid

Independent variable 3  
Temperature of Liquid

Units: K Uncertainty: 0.05 %

Definition of Measurement Results (Absolute vs Relative)  
Direct value

Data presentation  
Experimental values

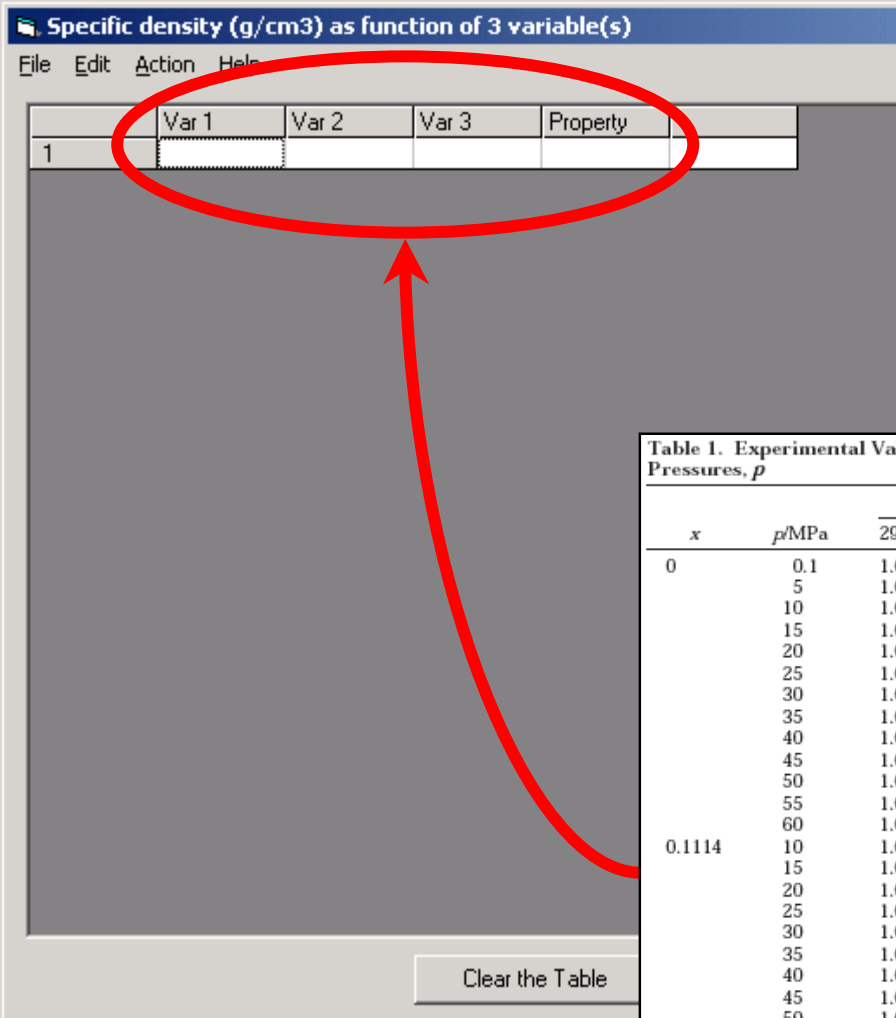
Comments (Optional):

Property and method Numerical Data Cancel

1. SELECT *Direct Value* (as compared with *Relative Value*) from the list defining the **Measurement Results**

2. SELECT the appropriate **Data presentation** method. *Experimental values* here.

3. CLICK *Numerical Data*



**TYPE, or much preferably, PASTE the variable and property values into the table. See next page...**

**Table 1. Experimental Values of Densities,  $\rho$ , for  $x$  HFC-134a + (1 -  $x$ ) TEGDME at Different Temperatures,  $T$ , and Pressures,  $p$**

$x$	$p$ /MPa	$\rho$ (g·cm <sup>-3</sup> ) at the following values of $T$ /K								
		293.15	303.15	313.15	323.15	333.15	343.15	353.15	363.15	373.15
0	0.1	1.0112	1.0018	0.9925	0.9833	0.9740	0.9648	0.9556	0.9469	0.9375
	5	1.0142	1.0050	0.9959	0.9868	0.9778	0.9687	0.9598	0.9513	0.9423
	10	1.0172	1.0082	0.9992	0.9903	0.9814	0.9726	0.9639	0.9557	0.9468
	15	1.0201	1.0113	1.0025	0.9937	0.9850	0.9764	0.9679	0.9598	0.9511
	20	1.0229	1.0143	1.0055	0.9970	0.9883	0.9800	0.9716	0.9639	0.9552
	25	1.0257	1.0172	1.0086	1.0001	0.9917	0.9835	0.9752	0.9675	0.9593
	30	1.0284	1.0200	1.0116	1.0032	0.9950	0.9869	0.9788	0.9712	0.9631
	35	1.0310	1.0227	1.0144	1.0063	0.9982	0.9901	0.9821	0.9748	0.9669
	40	1.0336	1.0254	1.0172	1.0091	1.0012	0.9932	0.9855	0.9783	0.9704
	45	1.0361	1.0281	1.0201	1.0121	1.0042	0.9963	0.9886	0.9815	0.9739
	50	1.0385	1.0306	1.0226	1.0147	1.0070	0.9993	0.9917	0.9846	0.9771
	55	1.0410	1.0332	1.0252	1.0175	1.0098	1.0023	0.9947	0.9880	0.9805
60	1.0434	1.0355	1.0278	1.0202	1.0126	1.0050	0.9976	0.9910	0.9838	
0.1114	10	1.0315	1.0220	1.0124	1.0031	0.9936	0.9844	0.9752	0.9659	0.9564
	15	1.0345	1.0254	1.0159	1.0067	0.9975	0.9887	0.9794	0.9704	0.9611
	20	1.0375	1.0285	1.0192	1.0103	1.0011	0.9925	0.9834	0.9746	0.9657
	25	1.0405	1.0316	1.0223	1.0136	1.0047	0.9962	0.9872	0.9787	0.9699
	30	1.0433	1.0346	1.0255	1.0169	1.0081	0.9998	0.9911	0.9828	0.9742
	35	1.0461	1.0374	1.0286	1.0201	1.0116	1.0032	0.9947	0.9866	0.9779
	40	1.0488	1.0403	1.0316	1.0232	1.0148	1.0065	0.9983	0.9903	0.9817
	45	1.0515	1.0431	1.0345	1.0263	1.0179	1.0099	1.0017	0.9937	0.9854
50	1.0541	1.0457	1.0374	1.0291	1.0210	1.0129	1.0050	0.9972	0.9890	
55	1.0567	1.0485	1.0401	1.0321	1.0241	1.0162	1.0083	1.0006	0.9926	
60	1.0593	1.0510	1.0430	1.0349	1.0269	1.0192	1.0114	1.0038	0.9955	
0.2896	10	1.0563	1.0460	1.0357	1.0255	1.0151	1.0050	0.9948	0.9847	0.9742
	15	1.0598	1.0497	1.0396	1.0296	1.0196	1.0097	0.9997	0.9899	0.9798
	20	1.0632	1.0533	1.0434	1.0337	1.0237	1.0142	1.0044	0.9948	0.9850
	25	1.0665	1.0568	1.0470	1.0375	1.0278	1.0185	1.0089	0.9995	0.9899
	30	1.0697	1.0601	1.0506	1.0412	1.0317	1.0225	1.0132	1.0039	0.9947
	35	1.0728	1.0634	1.0540	1.0447	1.0355	1.0265	1.0173	1.0083	0.9991
	40	1.0759	1.0666	1.0573	1.0482	1.0392	1.0303	1.0213	1.0125	1.0035
	45	1.0788	1.0697	1.0606	1.0517	1.0428	1.0339	1.0250	1.0164	1.0076
	50	1.0818	1.0727	1.0637	1.0548	1.0461	1.0374	1.0287	1.0203	1.0116
	55	1.0846	1.0757	1.0668	1.0581	1.0495	1.0410	1.0325	1.0241	1.0157
	60	1.0874	1.0785	1.0699	1.0613	1.0528	1.0443	1.0359	1.0277	1.0194

Specific density (g/cm<sup>3</sup>) as function of 3 variable(s)

File Edit Action Help

	Var 1	Var 2	Var 3	Property
1	0	0.1	293.15	1.0112
2	0	5	293.15	1.0142
3	0	10	293.15	1.0172
4	0	15	293.15	1.0201
5	0	20	293.15	1.0229
6	0	25	293.15	1.0257
7	0	30	293.15	1.0284
8	0	35	293.15	1.0310
9	0	40	293.15	1.0336
10	0	45	293.15	1.0361
11	0	50	293.15	1.0385
12	0	55	293.15	1.0410
13	0	60	293.15	1.0434
14	0	0.1	303.15	1.0018
15	0	5	303.15	1.0050
16	0	10	303.15	1.0082
17	0	15	303.15	1.0113
18	0	20	303.15	1.0143
19	0	25	303.15	1.0172
20	0	30	303.15	1.0200
21	0	35	303.15	1.0227
22	0	40	303.15	1.0254
23	0	45	303.15	1.0281
24	0	50	303.15	1.0306
25	0	55	303.15	1.0332

Clear the Table View p

Table 1. Experimental Values of Densities,  $\rho$ , for  $x$  HFC-134a + (1 -  $x$ ) TEGDME at Different Temperatures,  $T$ , and Pressures,  $p$

$x$	$p$ /MPa	$\rho$ (g·cm <sup>-3</sup> ) at the following values of $T$ /K								
		293.15	303.15	313.15	323.15	333.15	343.15	353.15	363.15	373.15
0	0.1	1.0112	1.0018	0.9925	0.9833	0.9740	0.9648	0.9556	0.9469	0.9375
	5	1.0142	1.0050	0.9959	0.9868	0.9778	0.9687	0.9598	0.9513	0.9423
	10	1.0172	1.0082	0.9992	0.9903	0.9814	0.9726	0.9639	0.9557	0.9468
	15	1.0201	1.0113	1.0025	0.9937	0.9850	0.9764	0.9679	0.9598	0.9511
	20	1.0229	1.0143	1.0055	0.9970	0.9883	0.9800	0.9716	0.9639	0.9552
	25	1.0257	1.0172	1.0086	1.0001	0.9917	0.9835	0.9752	0.9675	0.9593
	30	1.0284	1.0200	1.0116	1.0032	0.9950	0.9869	0.9788	0.9712	0.9631
	35	1.0310	1.0227	1.0144	1.0063	0.9982	0.9901	0.9821	0.9748	0.9669
	40	1.0336	1.0254	1.0172	1.0091	1.0012	0.9932	0.9855	0.9783	0.9704
	45	1.0361	1.0281	1.0201	1.0121	1.0042	0.9963	0.9886	0.9815	0.9739
0.1114	50	1.0385	1.0306	1.0226	1.0147	1.0070	0.9993	0.9917	0.9846	0.9771
	55	1.0410	1.0332	1.0252	1.0175	1.0098	1.0023	0.9947	0.9880	0.9805
	60	1.0434	1.0355	1.0278	1.0202	1.0126	1.0050	0.9976	0.9910	0.9838
	10	1.0315	1.0220	1.0124	1.0031	0.9936	0.9844	0.9752	0.9659	0.9564
	15	1.0345	1.0254	1.0159	1.0067	0.9975	0.9887	0.9794	0.9704	0.9611
	20	1.0375	1.0285	1.0192	1.0103	1.0011	0.9925	0.9834	0.9746	0.9657
	25	1.0405	1.0316	1.0223	1.0136	1.0047	0.9962	0.9872	0.9787	0.9699
	30	1.0433	1.0346	1.0255	1.0169	1.0081	0.9998	0.9911	0.9828	0.9742
	35	1.0461	1.0374	1.0286	1.0201	1.0116	1.0032	0.9947	0.9866	0.9779
	40	1.0488	1.0403	1.0316	1.0232	1.0148	1.0065	0.9983	0.9903	0.9817
0.2896	45	1.0515	1.0431	1.0345	1.0263	1.0179	1.0099	1.0017	0.9937	0.9854
	50	1.0541	1.0457	1.0374	1.0291	1.0210	1.0129	1.0050	0.9972	0.9890
	55	1.0567	1.0485	1.0401	1.0321	1.0241	1.0162	1.0083	1.0006	0.9926
	60	1.0593	1.0510	1.0430	1.0349	1.0269	1.0192	1.0114	1.0038	0.9955
	10	1.0563	1.0460	1.0357	1.0255	1.0151	1.0050	0.9948	0.9847	0.9742
	15	1.0598	1.0497	1.0396	1.0296	1.0196	1.0097	0.9997	0.9899	0.9798
	20	1.0632	1.0533	1.0434	1.0337	1.0237	1.0142	1.0044	0.9948	0.9850
	25	1.0665	1.0568	1.0470	1.0375	1.0278	1.0185	1.0089	0.9995	0.9899
	30	1.0697	1.0601	1.0506	1.0412	1.0317	1.0225	1.0132	1.0039	0.9947
	35	1.0728	1.0634	1.0540	1.0447	1.0355	1.0265	1.0173	1.0083	0.9991
40	1.0759	1.0666	1.0573	1.0482	1.0392	1.0303	1.0213	1.0125	1.0035	
45	1.0788	1.0697	1.0606	1.0517	1.0428	1.0339	1.0250	1.0164	1.0076	
50	1.0818	1.0727	1.0637	1.0548	1.0461	1.0374	1.0287	1.0203	1.0116	
55	1.0846	1.0757	1.0668	1.0581	1.0495	1.0410	1.0325	1.0241	1.0157	
60	1.0874	1.0785	1.0699	1.0613	1.0528	1.0443	1.0359	1.0277	1.0194	

**NOTE:** Simple CUT/PASTE procedures can be used within the table to convert the original table into the required number of columns. (This can also be done externally in spreadsheet software, e.g., EXCEL.)



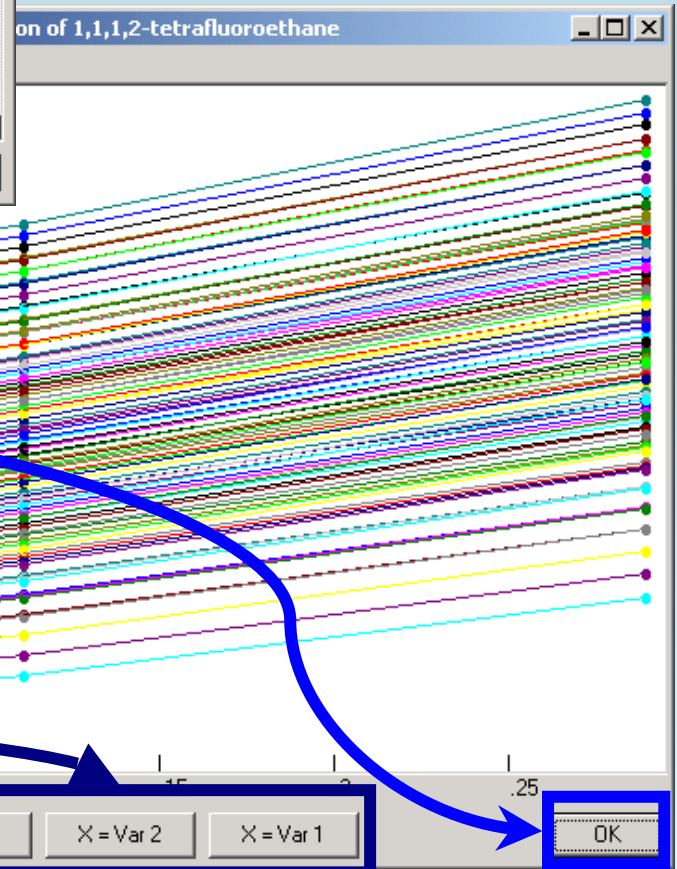
Specific density (g/cm<sup>3</sup>) as function of 3 variable(s)

File Edit Action Help

	Var 1	Var 2	Var 3	Property
1	0	0.1	293.15	1.0112
2	0	5	293.15	1.0142
3	0	10	293.15	1.0172
4	0	15	293.15	1.0201
5	0	20	293.15	1.0229
6	0	25	293.15	1.0257
7	0	30	293.15	1.0284
8	0	35	293.15	1.0310
9	0	40	293.15	1.0336
10	0	45	293.15	1.0361
11	0	50	293.15	1.0385
12	0	55	293.15	1.0410
13	0	60	293.15	1.0434
14	0	0.1	303.15	1.0018
15	0	5	303.15	1.0050
16	0	10	303.15	1.0082
17	0	15	303.15	1.0113
18	0	20	303.15	1.0143
19	0	25	303.15	1.0172
20	0	30	303.15	1.0200
21	0	35	303.15	1.0227
22	0	40	303.15	1.0254
23	0	45	303.15	1.0281
24	0	50	303.15	1.0306
25	0	55	303.15	1.0332

Clear the Table View plot Accept Cancel

1. CLICK *View plot* to see a graphical representation of the data.



2. Check for typographical errors, and CLICK *OK*, when done.

**NOTE:** These buttons provide different views of the data. See next screens

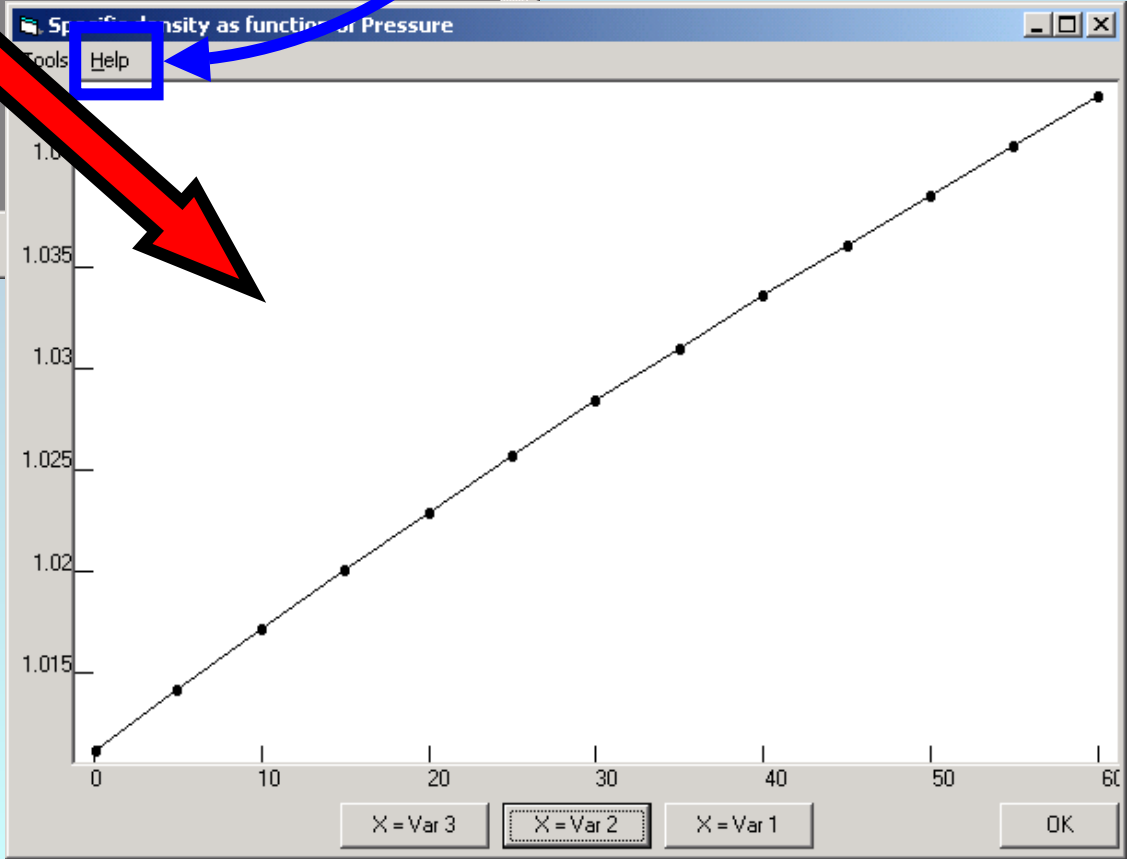
Specific density (g/cm<sup>3</sup>) as function of 3 variable(s)

File Edit Action Help

	Var 1	Var 2	Var 3	Property
1	0	0.1	293.15	1.0112
2	0	5	293.15	1.0142
3	0	10	293.15	1.0172
4	0	15	293.15	1.0201
5	0	20	293.15	1.0229
6	0	25	293.15	1.0257
7	0	30	293.15	1.0284
8	0	35	293.15	1.0310
9	0	40	293.15	1.0336
10	0	45	293.15	1.0361
11	0	50	293.15	1.0385
12	0	55	293.15	1.0410
13	0	60	293.15	1.0434
14	0	0.1	303.15	1.0018
15	0	5	303.15	1.0050
16	0	10	303.15	1.0082
17	0	15	303.15	1.0113
18	0	20	303.15	1.0143
19	0	25	303.15	1.0172
20	0	30	303.15	1.0200
21	0	35	303.15	1.0227
22	0	40	303.15	1.0254
23	0	45	303.15	1.0281
24	0	50	303.15	1.0306
25	0	55	303.15	1.0332

Clear the Table View plot

**NOTE:** See **HELP** for addition graph commands.



**NOTE:** By selecting only part of the data set in the table, clearer views can be obtained.

Specific density (g/cm<sup>3</sup>) as function of 3 variable(s)

File Edit Action Help

	Var 1	Var 2	Var 3	Property
1	0	0.1	293.15	1.0112
2	0	5	293.15	1.0142
3	0	10	293.15	1.0172
4	0	15	293.15	1.0201
5	0	20	293.15	1.0229
6	0	25	293.15	1.0257
7	0	30	293.15	1.0284
8	0	35	293.15	1.0310
9	0	40	293.15	1.0336
10	0	45	293.15	1.0361
11	0	50	293.15	1.0385
12	0	55	293.15	1.0410
13	0	60	293.15	1.0434
14	0	0.1	303.15	1.0018
15	0	5	303.15	1.0050
16	0	10	303.15	1.0082
17	0	15	303.15	1.0113
18	0	20	303.15	1.0143
19	0	25	303.15	1.0172
20	0	30	303.15	1.0200
21	0	35	303.15	1.0227
22	0	40	303.15	1.0254
23	0	45	303.15	1.0281
24	0	50	303.15	1.0306
25	0	55	303.15	1.0332

**CLICK *Accept***

Clear the Table View plot **Accept** Cancel

## Guided Data Capture - Thermophysical and Thermochemical Data

File Edit Tools Help

Reference

Compound

Sample

Mixture

Reaction

Property

2002 com bay 0

1,1,1,2-tetrafluoroethane

Sample 1 (cm,99.94x%,nc;ns;)

^2: VDN (L), Set 1, B Method:VIBTUB

2,5,8,11,14-pentaoxapentadecane

Sample 1 (cm,99x%,nc;ns;)

^2: VDN (L), Set 1, B Method:VIBTUB dVDN=0.0002 dP=50 dT=0.05

2,5,8,11,14-pentaoxapentadecane + 1,1,1,2-tetrafluoroethane

^3: VDN (Set 1), B Method:VIBTUB dVDN=0.0002 dP=0.05 dT=0.05

**NOTE:** The new data set now appears in the tree under the appropriate *mixture*.

**NOTE:** DOUBLE CLICKING on the *data set* allows editing of all entered information.

**END**

**Continue with other compounds,  
samples, properties, reactions, etc...**

***or* save your file and exit the program,  
if all properties have been captured.**